

2017 annual EDUG meeting, Lyon 22-23 June




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Adiabatic calorimetry – new trends
and some peculiarities of application
A. Kossoy

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Topics to be discussed

1. Types of adiabatic calorimeters
2. Something about theory and related problems
3. Phi-factor – what is usually supposed and what we have in reality
4. Study of energetic materials – is adiabatic calorimetry the right method?

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Types of adiabatic calorimeters

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- ✓ **Accelerating Rate Calorimeter**
 ARC - THT, NETZSCH (Germany)
 Phi-Tec I - HEL (UK)
- ✓ **Vent Sizing Package**
 VSP - FAI (USA)
 Phi-Tec II - HEL (UK)
- ✓ **New! Differential Accelerating Rate Calorimeter DARC - Omnicalc (USA)**
- ✓ **DEWAR**
 Mostly home-made
- ✓ **Advanced Reactive System**
 Screening Tool ARSST - FAI (USA)

Types of adiabatic calorimeters

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- ✓ **Accelerating Rate Calorimeter**
 ARC - THT, NETZSCH (Germany)
 Phi-Tec I - HEL (UK)
- ✓ **Vent Sizing Package**
 VSP - FAI (USA)
 Phi-Tec II - HEL (UK)
 Phi-Tec I - HEL (UK) (no P compensation)
- ✓ **Differential Accelerating Rate Calorimeter DARC - Omnicalc (USA)**
- ✓ **DEWAR**
 Chilworth (UK), home-made
- ✓ **Advanced Reactive System**
 Screening Tool ARSST - FAI (USA)

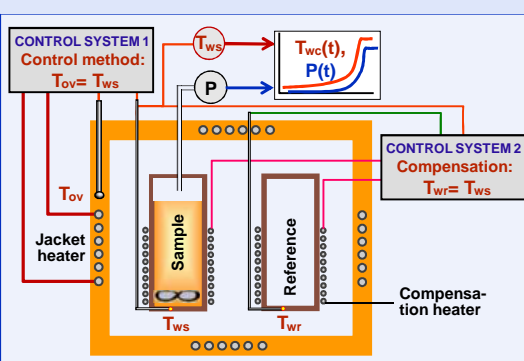
Types of adiabatic calorimeters



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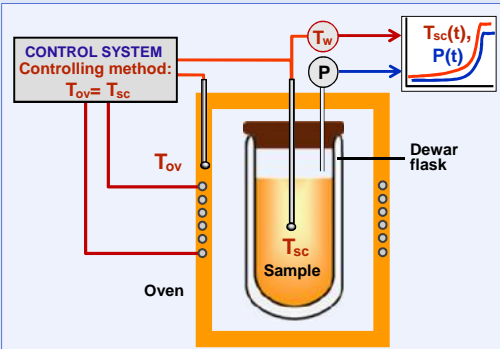
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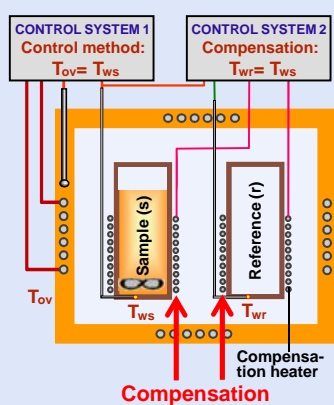
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Something about theory and related problems

Differential Accelerating Rate Calorimeter DARC, principle of the method ^{*)}


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1. $t=0, T=T_{onset}$ **Start of reaction. Heat release**
 $Q_r(0) = Q_r \dot{E} T_s = T_{onset} + Q_r / (C_s + C_w) \dot{E} T_{ws} - T_{wr} = UT_0$
2. **Compensation starts**
 $q_0 = C_w UT_0 \dot{E} T_{ws}$ increase $= q_0 / (C_s + C_w) = UT_I$
 $q_I = C_w UT_I = C_w q_0 / (C_s + C_w) = \{ q_0 = C_w \{ UT_0$
 $\{ = C_w q_0 / (C_s + C_w)$
3. **Cycle**
 $q_i = C_w UT_i = C_w \{ i UT_0, UT_i = \{ i UT_0$
 $\sum_{i=0}^n UT_i \dot{E} NUT_0 \sum_{i=0}^n \{ i NUT_0 \{ (1 > \{ n) \} \dot{E} UT_0 \{$

^{*)} Arata Kimura & Teruhito Otsuka, Performance evaluation of differential accelerating rate calorimeter for the thermal runaway reaction of di-tert-butyl peroxide, J Therm Anal Calorim (2013) V. 113:1585-1591

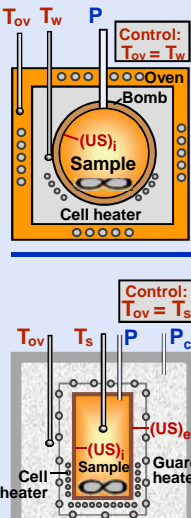
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Something about theory and related problems

Main assumption: Bomb and Sample are the uniform (lumped) systems

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$$c_b m_b \frac{dT_b}{dt} = (US)_i (T_s - T_b) - W_{loss};$$

$$c_s m_s \frac{dT_s}{dt} = W - (US)_i (T_s - T_b);$$

$$W = m_s \frac{dQ}{dt}$$

$c_s m_s \left\{ \frac{dT_s}{dt} = W; \{ = 1 + (c_b m_b) / (c_s m_s) \right.$

$$c_b m_b \frac{dT_b}{dt} = (US)_e (T_{ov} - T_b) + (US)_i (T_s - T_b) - W_{loss};$$


$$c_s m_s \frac{dT_s}{dt} = W - (US)_i (T_s - T_b);$$

\Downarrow

$$c_s m_s \frac{dT_s}{dt} + c_b m_b \frac{dT_b}{dt} = (US)_e (T_{ov} - T_b) + W - W_{loss};$$

$c_s m_s \left\{ \frac{dT_s}{dt} = W; \{ = 1 + (c_b m_b) / (c_s m_s) \right.$

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Something about theory and related problems

Assumption: Sample is in equilibrium with the Bomb (Ts=Tb) -??

1. ARC-type

$$c_b m_b \frac{dT_b}{dt} = (US)_i (T_s - T_b);$$

$$c_s m_s \frac{dT_s}{dt} = W - (US)_i (T_s - T_b);$$

⇒

$$c_s m_s \frac{dT_s}{dt} + c_b m_b \frac{dT_b}{dt} = W;$$

Simulation details

Bomb: stainless steel sphere, R=1.6 cm, wall thickness - 1 mm; $M_b=22.6$ g

Sample: low viscous liquid, $\rho = 1$ g/cm³; $C_p=2$ J/g/K; $M_s=13.6$ g; $\lambda=1.383$


Kinetics: 1-st order reaction; $K_0=5.32 \cdot 10^{11}$ 1/s; $E=120$ kJ/mol; $Q=400$ J/g

Internal heat transfer coefficient: $U=100$ W/m²/K

Boundary conditions:
adiabatic on the outer side of the bomb (ARC control method $T_{ov}=T_b$)

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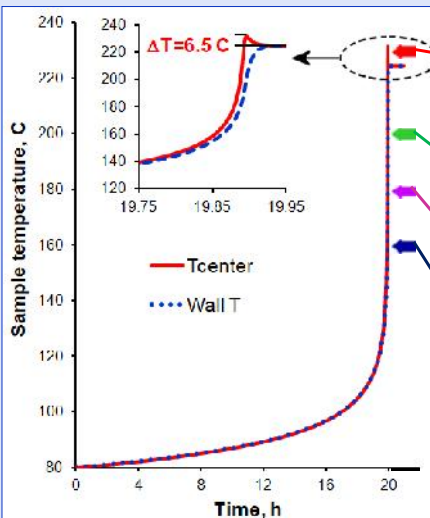
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Something about theory and related problems

Assumption: Sample is in equilibrium with the Bomb (Ts=Tb) -??

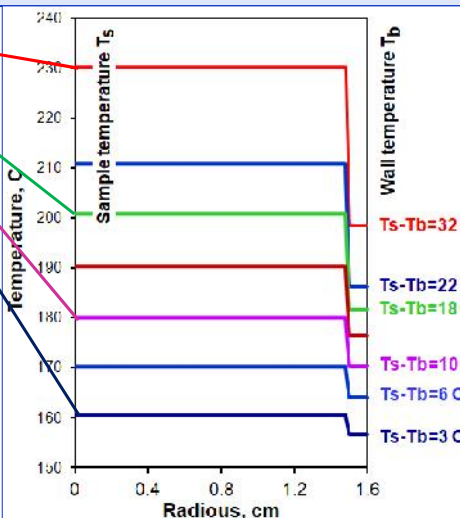


Sample temperature, C

Time, h

— Tcenter
••••• Wall T

$\Delta T = 6.5$ C



Sample temperature T_s


Wall temperature T_b

$T_s - T_b = 32$ C
 $T_s - T_b = 22$ C
 $T_s - T_b = 18$ C
 $T_s - T_b = 10$ C
 $T_s - T_b = 6$ C
 $T_s - T_b = 3$ C

Radius, cm

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Something about theory and related problems

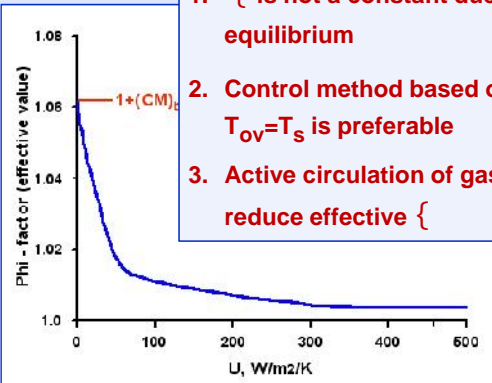
Assumption: Sample is in equilibrium with the Bomb (Ts=Tb) -??

2. VSP-type

$$c_b m_b \frac{dT_b}{dt} = (US)_e (T_{ov} - T_b) + (US)_i (T_s - T_b);$$


$$c_s m_s \frac{dT_s}{dt} = W - (US)_i (T_s - T_b);$$

1. $\{$ is not a constant due to deviation from equilibrium
2. Control method based on maintenance $T_{ov}=T_s$ is preferable
3. Active circulation of gas in the oven can reduce effective $\{$



$(US)_e (T_{ov} - T_b) + W;$
 $= T_s;$
 change

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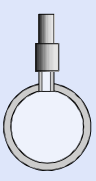

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Phi-factor – what is it really?


Thermal inertia $\{ \approx 1 + (c_b M_b)/(c_s M_s)$

Problem # 1 – how to determine thermal inertia?

What is bomb mass M_b =?



How to determine phi for DEWAR?




The best solution – calibration.
It is applied for DEWAR but not for other instruments

Why ?

Problem # 2 – how to minimize thermal inertia?

1. Reduce value of $c_b M_b$ – VSP, Phi-Tec II, DEWAR
2. Apply power-compensation – DARC
3. Apply advanced control method (e.g. gas circulation in the oven)
4. Apply math methods for phi correction

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Phi-factor – what is it really?

Thermal inertia $\{ \bar{\theta} 1 + (c_b M_b) / (c_s M_s) \}$

Problem # 3 – { - Constant or Variable ?

1st reason why { may vary:

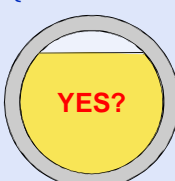
$C_b = f(T)$

$C_s = f(T, t)$: mixture composition varies in time

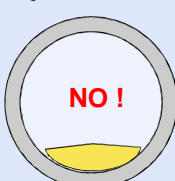
2nd reason why { may vary:

Lack of equilibrium between sample and bomb


$\{ \bar{\theta} \text{ Constant ?}$



$\{ \bar{\theta} \text{ Constant ?}$



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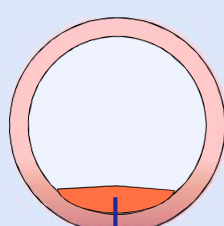

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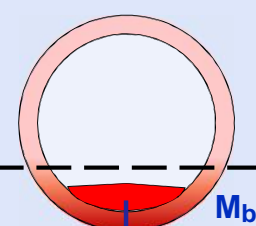
Phi-factor – what is it really?

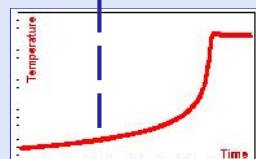
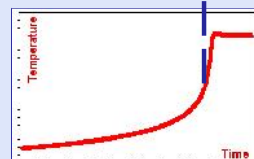
Thermal inertia $\{ \bar{\theta} 1 + (c_b M_b) / (c_s M_s) \}$

Problem # 3 – { - Constant or Variable ?


$\{ \bar{\theta} 1 + (c_b M_b) / (c_s M_s) \} \gg \{ \bar{\theta} 1 + (c_b M_{b,eff}) / (c_s M_s) \} !!$





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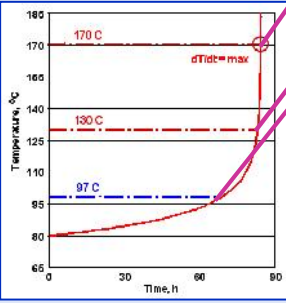
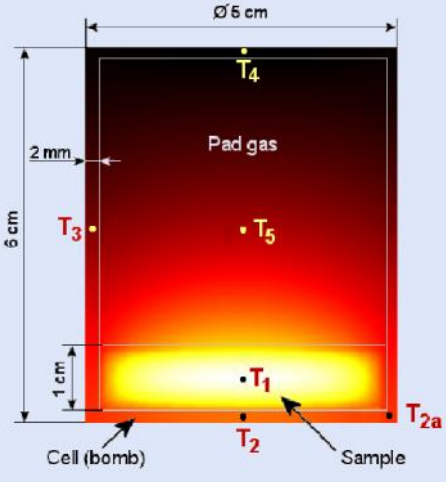

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Phi-factor – what is it really?


Thermal inertia $\{ \hat{0} 1 + (c_b M_b)/(c_s M_s) \}$

Problem # 3 – { - Constant or Variable ?

T2, C	T2a, C	T3, C	T4, C	T5, C	T _{max} =T1, C
156.8	155	151	148	151	170
126.5	126.3	125.7	125.1	125.8	130
97.21	97.2	97.13	97.1	97.2	97.33

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Applying adiabatic calorimetry for energetic materials

Main Problem - high energy release

Conditions of ARC experiment:

- Bomb mass ~22 g; bomb Cp~0.5 J/g/K
- Sample mass ~10 g; sample Cp~2 J/g/K
- $\{ =1.55$

Typical reactive mixture: Reaction heat - 2000~6000 J/g

- Max temperature rise - 70 ~200 C
- Max SHR~100 K/min

Energetic material: Reaction heat - 1000~3000 J/g

- Max temperature rise - 350 ~950 C and more!
- Max SHR~600 ~1000 K/min and more!

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Applying adiabatic calorimetry for energetic materials

Main Problem - high energy release

What to do? Increase { :

Bomb mass ~22 g; bomb Cp~0.5 J/g/K

Sample mass ~x g; sample Cp~2 J/g/K

Energetic material: Reaction heat – 2000, 3000 and 4000 J/g

Max temperature rise: keep ~300 – 340 C

Max SHR ??

Q, J/g	Ms, g	{	UTmax
2000	1	6.5	~300
3000	0.6	10.2	~300
4000	0.45	13.2	~300

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Applying adiabatic calorimetry for energetic materials


Main Problem - high energy release

Real example:

Phi-Tec I. Energetic material:

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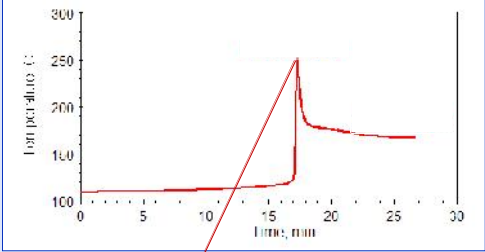
Applying adiabatic calorimetry for energetic materials

Main Problem - high energy release

Real example:

Phi-Tec I, Energetic material:


Bomb mass - 24.4 g;
bomb Cp - 0.42 J/g/K
Sample mass - 0.5 g;
Sample Cp - 2 J/g/K
 { =11



Q=1255 J/g if {_{eff} ~ 4: about 36% of calculated value

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Conclusions

1. **Adiabatic calorimetry:**
 - is known for almost 50 years
 - showed its usefulness
 - Is used extensively everywhere
2. **Nevertheless:**
 - still a lot of methodical problems
 - they must be resolved
3. **Application of the method to energetic materials:**
 - Is doomed to failure without applying specialized methods
 - no such methods are available at the moment


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Thank you
for your
attention!

Comments? 

Questions? 

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